

# A Literature Review on Air Side Heat Exchanger Fouling in Heating, Ventilation and Air-Conditioning (HVAC) Applications

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# Introduction

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- Extensive use of air to refrigerant heat exchangers in residential, commercial and industrial applications.
- Increased interest in the use of air cooled systems as an alternative to water cooled systems.
- Due to extensive use of air cooled heat exchangers in HVAC applications, It is important to analyze the fouling phenomenon in these systems.



# Introduction

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- Fouling mechanisms and agents
  - » Accumulation and growth of particles on heat exchanger (HX) surface.
  - » Inorganic materials as well as organic materials.
  - » Dependent on HX design and particular process in which it is used.
- Fouling effects
  - » Decrease in heat transfer.
  - » Hindrance to air flow - increase in air side pressure drop.
  - » Increases fan power.



# Fouling Phenomenon

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- Fouling phenomenon can be divided into (Awad,2011):
  - » Particulate fouling  
Accumulation of suspended particles in the fluid stream on the heat exchanger surface.
  - » Precipitate fouling  
Due to the presence of dissolved salts in the saturated solution.
  - » Chemical reaction fouling  
Due to the chemical reaction that takes place between the particles present in the fluid stream. Heat exchanger surface can act as a catalyst.

BC1  
LU7

## Slide 4

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**BC1**

does this include reaction with the surface? What about corrosion?

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**LU7**

corrosion is seperately listed

Lab User, 6/29/2016



# Fouling Phenomenon

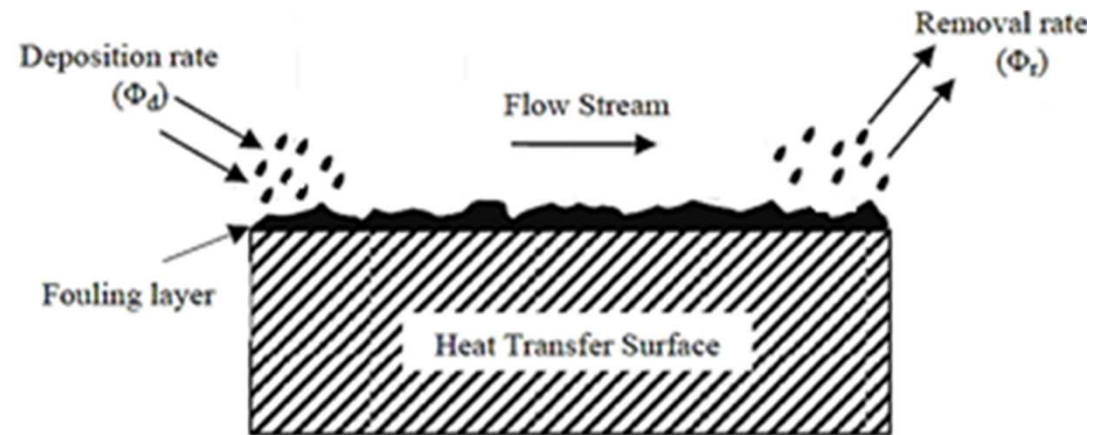
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- Fouling phenomenon can be divided into (Awad,2011):
  - » Corrosion fouling  
Due to electrochemical reactions that can take place between heat transfer surface and fluid stream.
  - » Biological fouling  
Due to the presence of biological matter in the fluid stream.
  - » Freezing fouling/Frosting  
Due to the freezing of liquid on heat transfer surface like frosting of heat exchangers during winter.



# Fouling Phenomenon

- Main fouling mechanisms, air-cooled heat exchangers (Siegel & Nazaroff, 2003):
  - » Particulate fouling,
  - » Biological fouling,
  - » Freezing fouling.



*Fouling Process (Awad, 2011)*

- The fouling rate is the difference between deposition rate,  $\Phi_d$  and removal rate,  $\Phi_r$  (Awad, 2011)



# Fouling Phenomenon

- Siegel & Nazaroff (2003) developed a model for the particles deposition onto the heat transfer surface.
- The overall deposition fraction  $\eta$  is: RC3  
LU2

$$\eta = 1 - P_{\text{fin}} \cdot P_{\text{tube}} \cdot P_G \cdot P_T \cdot P_D$$

where:

- »  $P_{\text{fin}}$  = Particles fraction lost due to impaction on fin edges,
- »  $P_{\text{tube}}$  = Particles fraction lost due to deposition on tube surface,
- »  $P_G$  = Particles fraction lost due to gravitational settling,
- »  $P_T$  = Particles RC2  
LU1 fraction lost due to deposition by turbulence, and
- »  $P_D$  = Particles fraction lost due to the due to Brownian motion.



## Slide 7

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**BC2** is this length or diameter if we talk about fibrous fouling?

Bach, Christian, 6/29/2016

**LU1** diameter

Lab User, 6/29/2016

**BC3** The reader has no idea what the different P's are. Please add below the formula. You might need to split the slide up into two slides. A lot of text already

Bach, Christian, 6/29/2016

**LU2** added

Lab User, 6/29/2016



# Fouling Phenomenon

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- Strong function of particle size but a weak function of air velocity and fin spacing.
- Dominating mechanisms by particle size:
  - » (0.01-1  $\mu\text{m}$ ) deposited by Brownian diffusion.
  - » (1-10  $\mu\text{m}$ ) deposited by impaction on fin edges.
  - » (>10  $\mu\text{m}$ ) deposited by air turbulence, impaction on tubes and gravitational settling.



# Biofouling

- Two types of <sup>RC4</sup><sub>LU4</sub> fouling commonly found in literature for air cooled heat exchangers:
  - » Biofouling, and
  - » Air dust deposition.
- Biofouling
  - » Biological matter in the air stream
  - » Microorganisms flourish in prolonged presence of water on surface of heat exchangers.
- Effect of biofouling on the performance of the heat exchangers was studied by Pu *et al.* (2009).
  - » Results see next slide

## Slide 9

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**BC4**

This contradicts some of your previous slides, including slide 5

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**LU4**

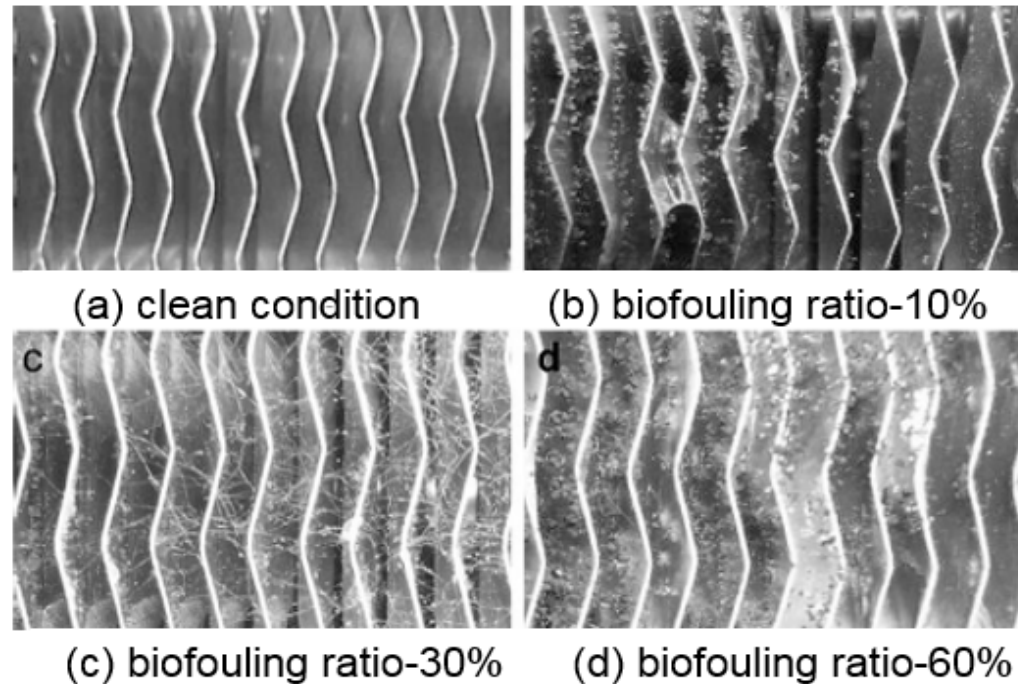
biofouling-->biological fouling , and air dust deposition--> particulate fouling

Lab User, 6/29/2016



# Biofouling

- Biofouling causes hydrophilic coating on heat exchanger surface to fail.
- For 2 m/s air velocity
  - » Heat transfer coefficient decreased by 7.2% and 15.9 % for a biofouled area ratio of 10% and 60 % respectively.
  - » Pressure drop increased by 43.1% for a biofouled area ratio of 60% .



*Heat exchangers during biofouling test  
with *Aspergillus niger* (Pu et al. 2009)*



# Air Dust Deposition Fouling



- Various researchers studied the dust deposition fouling for different heat exchangers.

Source	Heat exchanger type	Dust type	Amount of injected dust	Heat exchanger face area
Ali & Ismail (2008)	Plate fin-and-tube	From used field installed evaporators	300 g	0.048 m <sup>2</sup>
Ahn <i>et al.</i> (2003)	Fin and tube	Heat exchanger samples from field	Not applicable since field units were tested	No information given
Bell & Groll (2010)	Microchannel & Plate fin	ASHRAE standard dust & Arizona road test dust	300 g	0.2 m <sup>2</sup>
Yang <i>et al.</i> (2007)	Wavy fin and Lanced fin	No dust (Strip of paper to simulate fouling)	Not Applicable	0.372 m <sup>2</sup>
Pak <i>et al.</i> (2003)	Plate fin and Spine fin	ASHRAE standard dust	300 g	No information given
Qureshi & Zubair (2011)	Plate fin	Not applicable (model developed using EES)	Not applicable	No information given

- Air-side fouling depends on a number of factors on the heat exchanger (system) side and the air-side.



# Air Dust Deposition Fouling



- In HVAC systems, fin & tube heat exchanger are extensively used for residential, commercial, and industrial applications.
- For the fin and tube exchangers, airside fouling is dependent on:
  - » Fin type,
  - » Number of tube rows,
  - » Heat exchanger type,
  - » Fin spacing,
  - » Refrigerant type, and
  - » Filters, if any.

RC  
LUS

## Slide 12

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**BC6**

I think you already established this in the beginning, need to mention it here again?

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**LU5**

emphasis on fin and tube exchangers, literature review is for fin and tube exchangers

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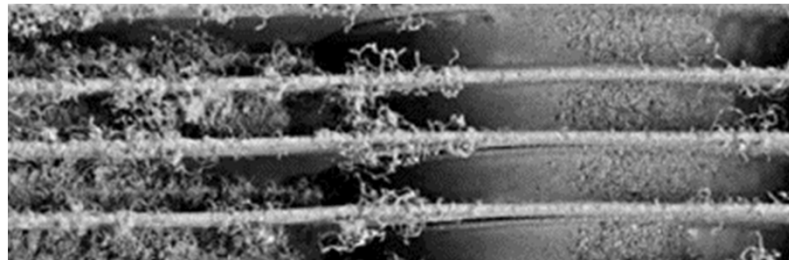




# Air Dust Deposition Fouling

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- Air dust fouling is more severe on the front face than the rear face [(Pak *et al.*, 2005) & (Ali & Ismail, 2008)].
- On the frontal face, dust accumulates on the leading edges



*Front face of coil fouled with 600g of injected dust. (Bell *et al.*, 2011)*

- Pak *et al.* (2005) found that out of the total amount of dust injected, amount of dust accumulated on single row condenser was 30-50% and 60-67% on double row BC7 condenser.
  - » The relative increase in pressure drop was almost identical for double and single row condenser.

**Slide 13**

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**BC7**

30-50% accumulated at front of HX? not clear...

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# Air Dust Deposition Fouling



- The performance of microchannel heat exchanger is more severely affected than plate & fin exchangers (Bell & Groll, 2010).
- Qureshi & Zubair (2011) conducted simulations with vapor BC8 compression refrigeration system model.
- The percentage decrease in the  $UA$  value due to air-side fouling was varied from 0% (*clean*) to 50% for heat exchanger.
- 3 different cases were considered:
  - » Condenser only fouling,
  - » Evaporator only fouling,
  - » Combined evaporator and condenser fouling.

**Slide 14**

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**BC8**

What model? The audience has no clue if this is a deposition model or a simple 4 component model with some factors for fouling

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# Air Dust Deposition Fouling



- Coefficient of performance (COP) of the condenser only fouling case was lower than evaporator only fouling.
- COP in the combined case was lower than other two cases.
- Yang *et al.* (2007) analyzed the cooling efficiency of packaged air conditioners equipped with filters for minimum efficiency reporting value (MERV) 4 to MERV 14.
  - » Energy efficiency ratio (EER) of the system for both clean and fouled case is reduced significantly by high-efficiency filters.



# Air Dust Deposition Fouling



- Siegel *et al.* (2002) analyzed residential evaporator coil performance by presenting a fin and tube heat exchanger fouling model.

» The mass concentration distribution function  $m_c$ , is

$$m_c = P_d (1 - \eta_f + \eta_f b_f) \cdot \eta_c \cdot (1 - b_c) \cdot m_{in}$$

where:

- $P_d$  = Particles fraction not removed by deposition in the duct work,
- $\eta_f$  = Filter efficiency calculated using ASHRAE standard 52.2
- $b_f$  = Filter bypass
- $\eta_c$  = Coil deposition fraction, and
- $m_{in}$  = Indoor particle distribution function



# Air Dust Deposition Fouling

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- Fouling time,  $\tau_{foul}$  is the time taken to double the pressure drop across the heat exchanger coil for a given air flow rate:

$$\tau_{foul} = \frac{M_{foul}}{Q M_c DC},$$

- »  $Q$  = Air flow rate through the system
  - »  $DC$  = Duty cycle of the air handler fan
  - »  $M_{foul}$  = Deposited mass for pressure drop of coil to double.
- $M_c$  is the total mass distribution that deposits in the coil:

$$M_c = \int_{d_p} m_c dd_p$$

- »  $d_p$  is the particle diameter and ranges from .01-100  $\mu\text{m}$ .



# Air Dust Deposition Fouling



- Fouling time ratio is the ratio of fouling time of a particular case in comparison to the base case.
- Average fouling time for the base case was 7.6 years.

*Fouling time ratios (Siegel et al. 2002)*

Variable	Base Case	Going to	Fouling Time Ratio		
			Median	GM	GSD
Filter Efficiency	MERV 2	MERV 6	1.39	1.39	1.08
		MERV 12	10.04	6.89	2.79
Indoor Concentration	Urban	Rural	0.43	0.45	1.23
	Cycling	CA	0.31	0.30	1.09
	Dirty	Clean	1.85	1.70	1.45
Coil Efficiency	4.7 fin/cm	2.4 fin/cm	1.82	1.90	1.11
		7.1 fin/cm	0.71	0.70	1.05
Filter Bypass	10%	None	1.81	1.12	2.26
		25%	0.73	0.86	1.38
Duct Penetration	Typical	Simple	0.99	0.99	1.01
		Complex	1.02	1.02	1.01

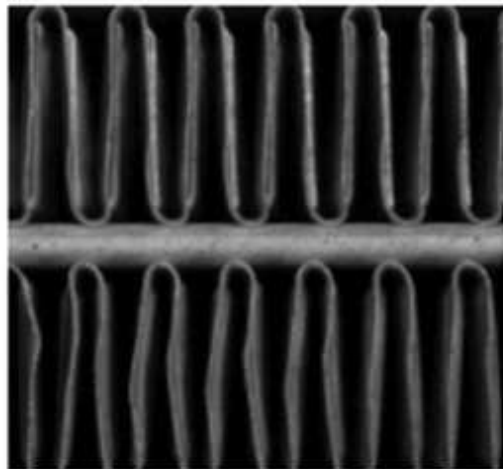




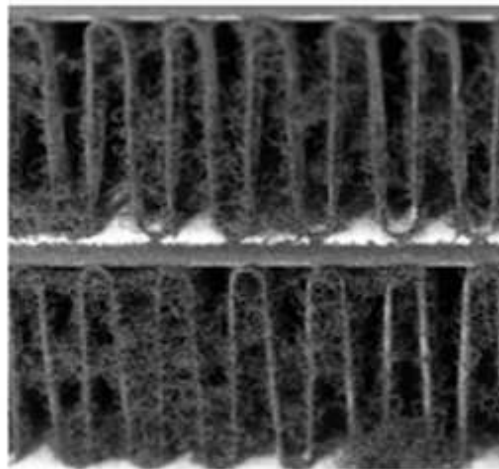
# Air Dust Deposition Fouling



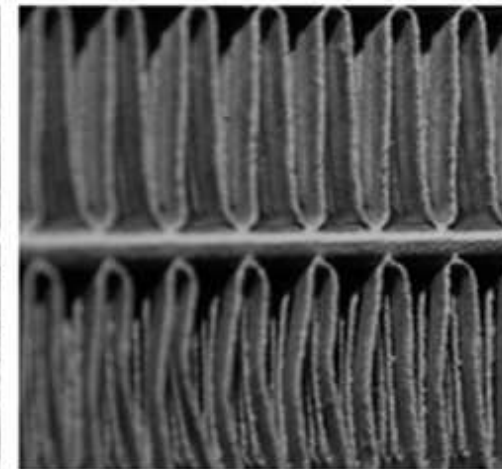
- Bell & Groll (2010) investigated heat exchangers performance using two fouling agents:
  - » ASHRAE standard dust (ASHRAE standard 52.1), includes fibrous matter.
  - » Arizona road test dust (particles only) as limiting case for fouling in the areas with little fibrous matter.



*(a) Clean condition*



*(b) Fouled with 135g of ASHRAE test dust*



*(c) Fouled with 500g of Arizona Road test dust*



# Air Dust Deposition Fouling



- Bell & Groll (2010) investigated the performance of heat exchangers using two different types of dust.
  - » The pressure drop for heat exchanger fouled with ASHRAE test standard dust was larger than Arizona test dust.
  - » Heat transfer reduced more in case of Arizona test dust due to its low thermal conductivity.
- Ali & Ismail (2008) used fouling material collected from evaporators that were put in their actual application.
  - » Sieve analysis was used to determine that particles ranged in size from 0.01 to 200  $\mu\text{m}$ .
  - » The fouling rate was found to be a strong function of air velocity.
  - » COP increased with the increase in air velocity in both the clean and fouled cases.



# Conclusion

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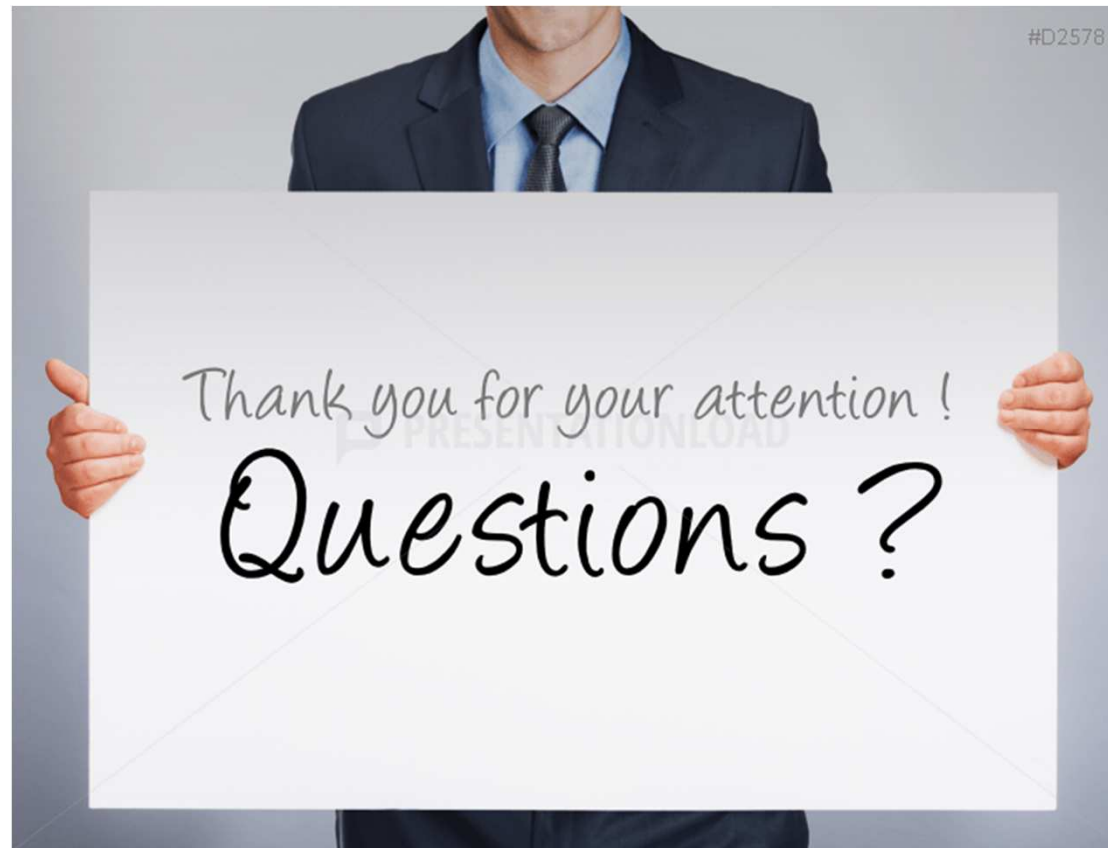
- A literature review of fouling in heat exchangers focused on air conditioning applications is presented.
- Fouling is more severe on the front face as compared to the rear face.
- The impact of fouling in increasing pressure drop for constant air flowrate is greater than the decrease in heat transfer.
  - » **Exception is particulate fouling with no fibrous matter**
- Using high-efficiency filters before evaporators causes an increase in fouling time.
- Increase in COP with an increase in air velocity for both the fouled and clean cases.



# References

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- Bell, I. H., & Groll, E. A. (2010). Experimental comparison of the impact of air-side particulate fouling on the thermo-hydraulic performance of microchannel and plate-fin heat exchangers. *International Refrigeration and Air Conditioning Conference*.



#D2578 BC12

## Slide 23

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### BC12

This looks like a picture from a website. Needs a citation! Suggest you follow my old example and just put in the first slide with fading in a semi-transparent black surface in front of it.

Bach, Christian, 6/29/2016